SYNERGY ENERGETICS®
Technological Research Investment Corp

EXECUTIVE SUMMARY

of a

TCG-UC EL500 W2GE Project

Based on

„Thermo-Chemical Gasification Technology"

– that utilizes Municipal Solid Waste and/or
„sewage sludge", its residuals, and other carboniferous wastes and materials
- in an environmental-friendly way -, in a closed, zero-emission Thermo-Degradation system,
for generating clean energy.

2016

Technical background

The Thermo-Chemical Gasification Technology – TCG - allows high temperature thermo chemical gasification without oxygen and air.

It incorporates several new technological developments and design features such as:

- modular construction and shop fabrication;
- no requirement for refractory brick;
- no requirement for separation and injection of oxygen;
- no sensitivity to moisture content in the feedstock;
- no requirement for pulverization or slurry injection of feed;
- flexibility in feedstock alternatives including varying proportions of coal, pet coke, biomass, sewer sludge or other organic waste in different proportions;
- utilization of a unique ionized water treatment system;
- capability of recycling un-reacted carbons back into the reactor chamber, and a near-zero air emissions and liquid discharge.

In addition, some of the carbon dioxide generated in the gasification process can be captured and recycled as feedstock. Further the potential exists to readily integrate this system into a portable, flexible gas-to-liquids bio-refinery. There is substantial commercial potential in the TCG unit.

During the last years, many novel design aspects have been further developed that culminated in a US patent filed on April 11, 2006, application No: 60 / 791,401.

The „TCG-UC System" covers the whole problem area, offering the total solution from the grinding machine, via the TCG Unit, to the „SECU" - SynGas-Electricity energy Conversion Unit (Gas motors or Turbines,) - to the „LFU" - Liquid Fuel Unit (Fischer-Tropsch or other Liquefaction technology) with a specific readily available additional equipment.

A solid carbonaceous material synthesis gas generation plant (gasifier) was built on a test site. This commercial scale reference plant was completed in mid-August 2007. Currently conducting operational start-up activities at the University of Toledo, Ohio. The plant is designed to utilize carbonaceous feedstock from coal to biomass including wood chips, rice straw, ethanol plant DDGS, and municipal and industry waste products (i.e. organic sludge, industry waste, petroleum coke) for synthesis gas production. The plant feed system is designed to handle blended feedstock, including coal mixed in any proportion, with the above mentioned materials.

From the middle of 2007, on the Denver, Colorado site, with a daily processing load of 75-200 tons of input material, the TCG installation met and in many cases exceeded the expectations suggested by our modeling and calculations.

The verification of these and other results was done by independent organizations. "***TSS Consultants"*** (http://www.tssconsultants.com) examined the potential and performance parameters of this thermo-chemical technology from a number of different angles. Five categories (E1-E5) were created and examined:

1. Economic viability (E1)

2. Energy Efficiency (E2)
3. Environmental Compatibility (E3)
4. Research, Development, Demonstration and Deployment (RDD&D) Evaluation Stages (E4)
5. Potential Socio-Political Effectiveness (E5)

These categories were selected and rated using data from several hundred installations worldwide either currently operational or in the planning stages.

After lengthy investigation, the analysts deemed the TCG installation to be the most highly rated, and further recommended it to the United States Senate as one of the foremost methods available today for reducing the importance of fossil fuels in energy generation in a most environmentally-friendly and safe manner.

TSS Consultants concluded that the

„TC thermo-chemical pyrolysis/steam refining process when conducted in absence of oxygen or air is superior to all other existing technologies examined."

The US House of Representatives, Science and Technology Committee, Subcommittee on Energy and Environment had requested testimony on research and development issues for producing liquid fuels from coal on September 5, 2007. Nationally and internationally recognized environmental scientists and researchers such as Mr. Bartis from RAND Corporation and Dr. Boardman from Idaho National Laboratory testified on the importance of this very issue.

The committee unanimously recommended to the federal government for support research on coal gasification and associated synthesis gas cleaning and treatment processes. These programs are near-term, relatively low risk concepts related mostly for power generation and hydrogen production. That said, many of the programs are also applicable to Fischer-Tropsch (F-T) technology to liquid fuels.

Specific Technology Innovations that are incorporated in the TCG-UC system

- Water Vapor (steam) is added into the system after the water has been super-saturated with negatively charged oxygen using patented water treatment technology (ionized steam reformation)
- Syngas is cooled by quenching with water which is then treated using patented technology to remove all tars and phenols, which are then recycled back into the gasifier. (gas clean-up)
- Partially decomposed particles are recycled through the system to achieve higher reaction efficiency. (carbon re-cycle)

- System operates at lower temperatures, (below vitrification levels) which requires less parasitic load and thus creates higher efficiency (non-slagging gasifier)
- Combustion flu gas can be captured and recycled, with minimal emissions.
- Final ash from system is generally not leachable, or can be contained in cementaciousbyproducts. (non-hazardous)
- Elimination of reactor refractory brick.

The feedstock

Although any carbon-based or carbonaceous material is suitable for use as an input material, the System achieves optimal efficiency when operated with mixed-source input materials. The System is capable of operating normally using single-source input material, however in this case its efficiency is dependent upon several factors.

ANY CARBONIFEROUS MATERIALS CAN BE USED IN THE TCG UNIT

In the projects, listed below we have modeled, - and is based on - a basic operation, using Municipal Solid Waste (MSW) and Sewage Sludge (SeSl), considering the existing incentive systems related to the MSW handling and sewage water cleaning.

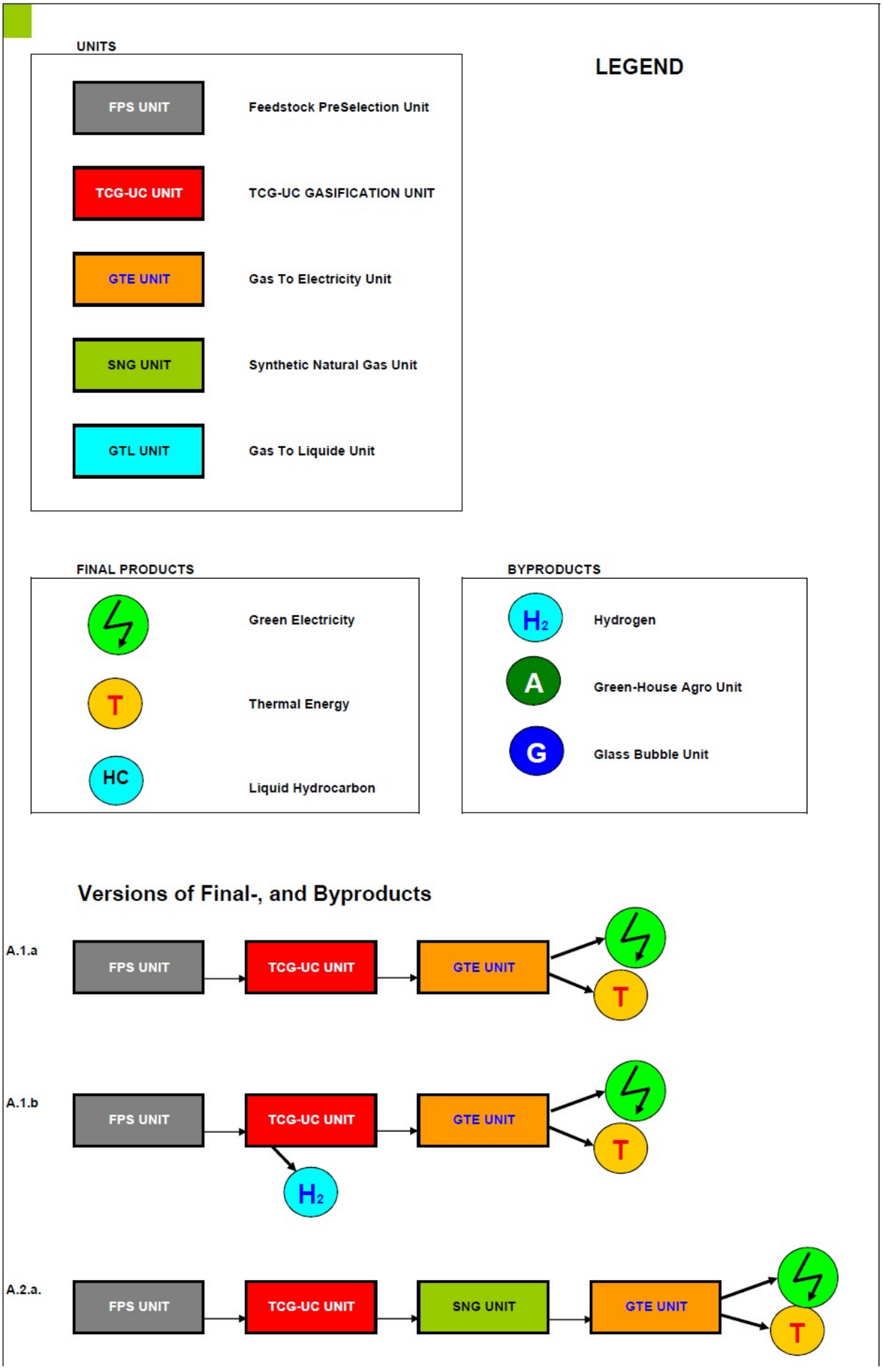
The European Union produces altogether cca 2 billion tons of MSW yearly. This mass of MSW contains about $2{,}4x10^{10}$ GJ ($6{,}6666x10^{9}$ MWh) energy.

This can be transformed to synthesys gas with $4{,}662x10^{9}$ MWh energy content.

The Output and Environmental protecting

- Syngas (which is itself a feedstock for any further processes and/or energy generation)
- slag/ash, dependent upon the ash content of the input materials, which is generated at an approximate rate of 2-25 tons per day. It is powdery and gray in color, environmentally-inactive, bound and water-insoluble, and is non-polluting. It is easily and beneficially integrated into construction, cement-making, or road construction applications, among many others depending upon the feedstock material.

There are no other liquid or gaseous emissions or environmental pollutants whatsoever formed by the TCG Unit and its processes


UNITS
LEGEND
FPS UNIT
Feedstock PreSelection Unit
TCG-UC UNIT
TCG-UC GASIFICATION UNIT
GTE UNIT
Gas To Electricity Unit
SNG UNIT
Synthetic Natural Gas Unit
GTL UNIT
Gas To Liquide Unit
FINAL PRODUCTS
Green Electricity
T
Thermal Energy
HC
Liquid Hydrocarbon
BYPRODUCTS
H2
Hydrogen
A
Green-House Agro Unit
G
Glass Bubble Unit
Versions of Final-, and Byproducts
A.1.a
FPS UNIT
TCG-UC UNIT
GTE UNIT
T
A.1.b
FPS UNIT
TCG-UC UNIT
GTE UNIT
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H2
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FPS UNIT
TCG-UC UNIT
SNG UNIT
GTE UNIT
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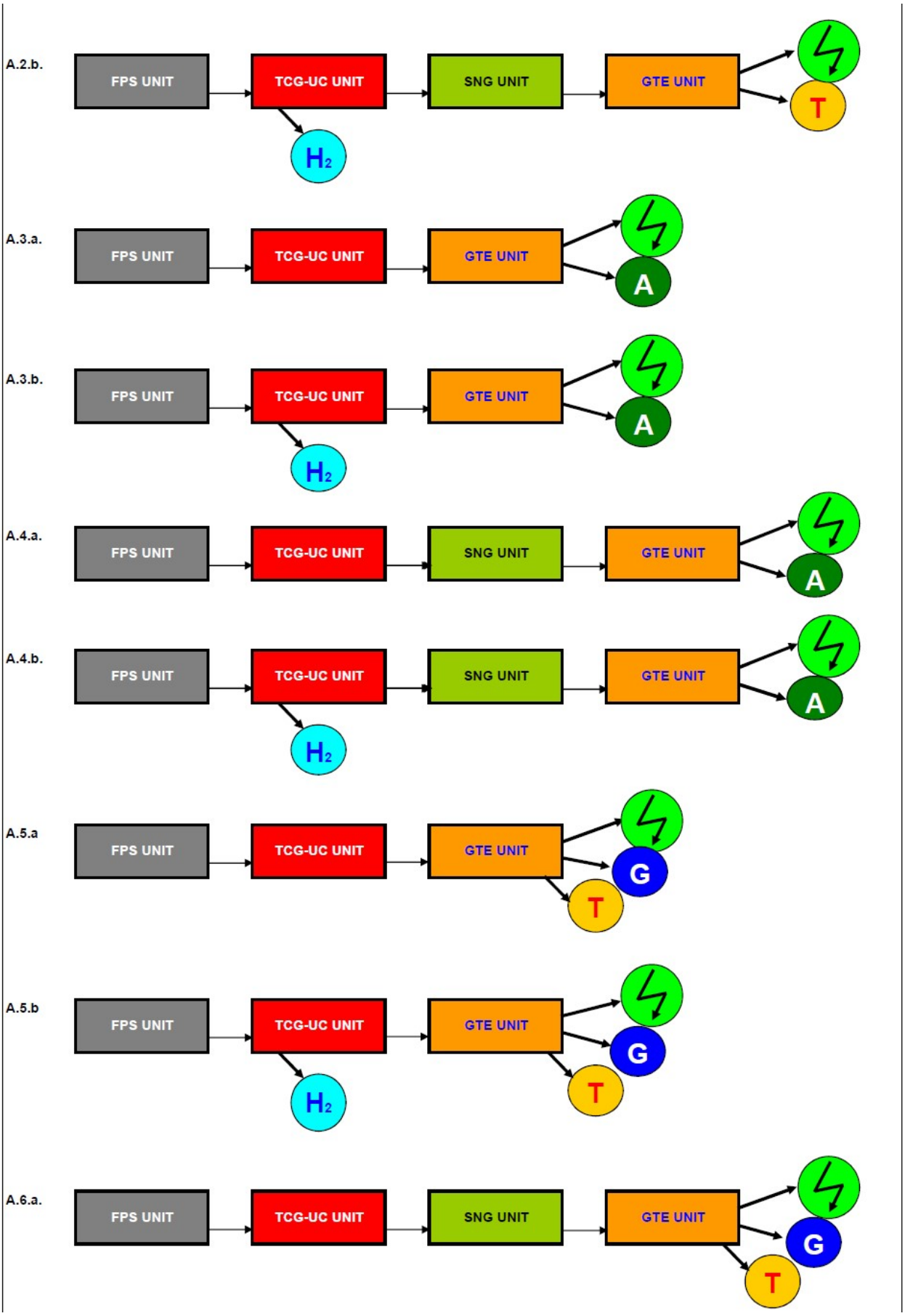
A.2.b.
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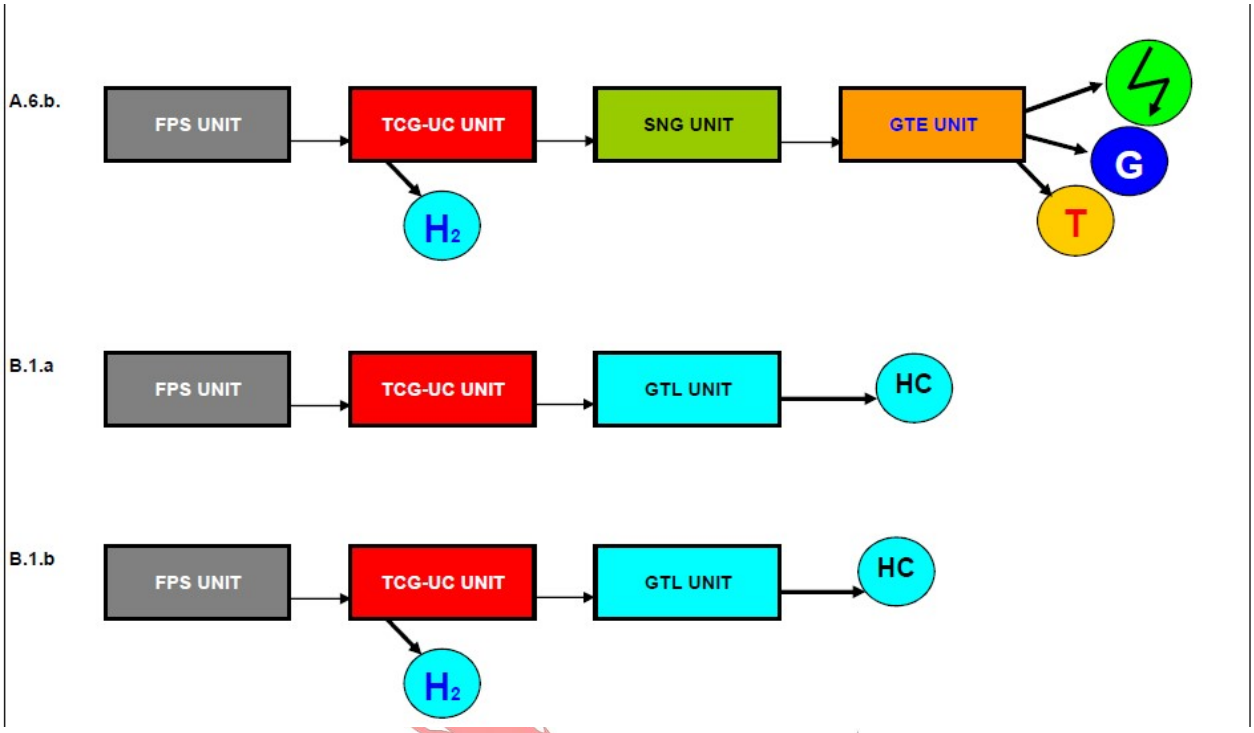
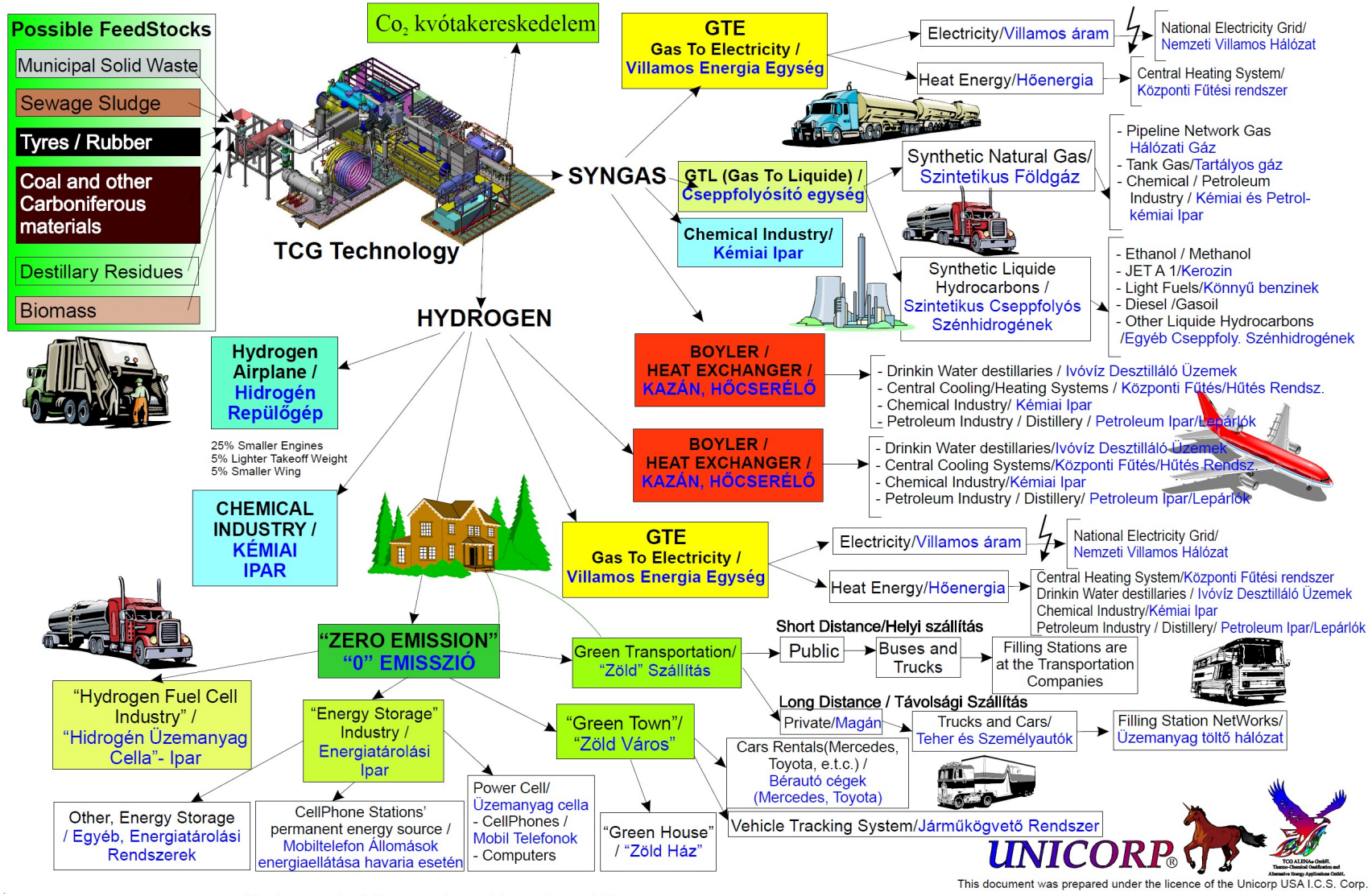
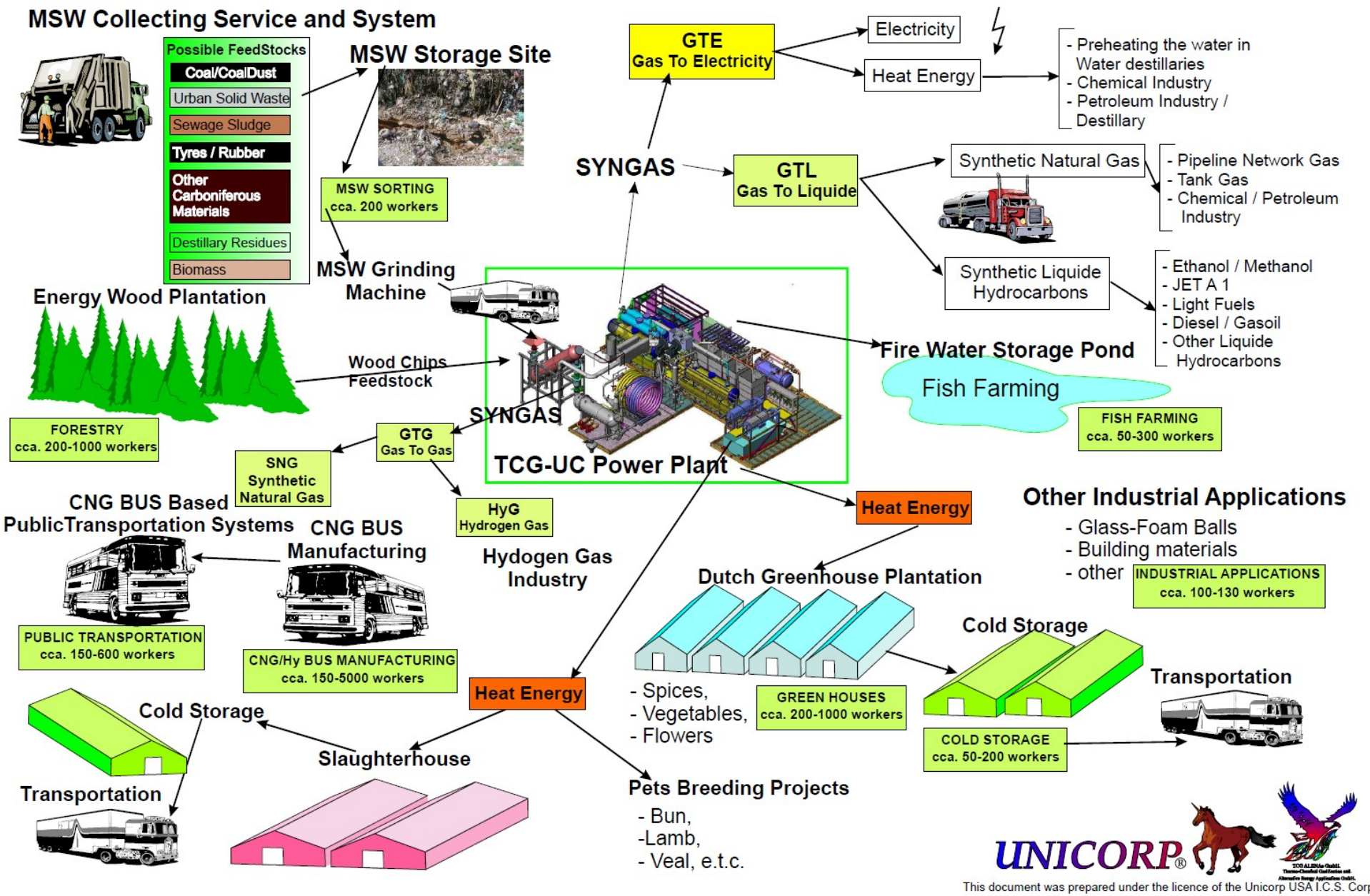


http://www.synergytri.eu/en/tcg_technology-id23.html

General Overview on the applications of SynGas/Hydrogen and the TCG Technology





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Process diagram of TCG-UC EL 500 Plant

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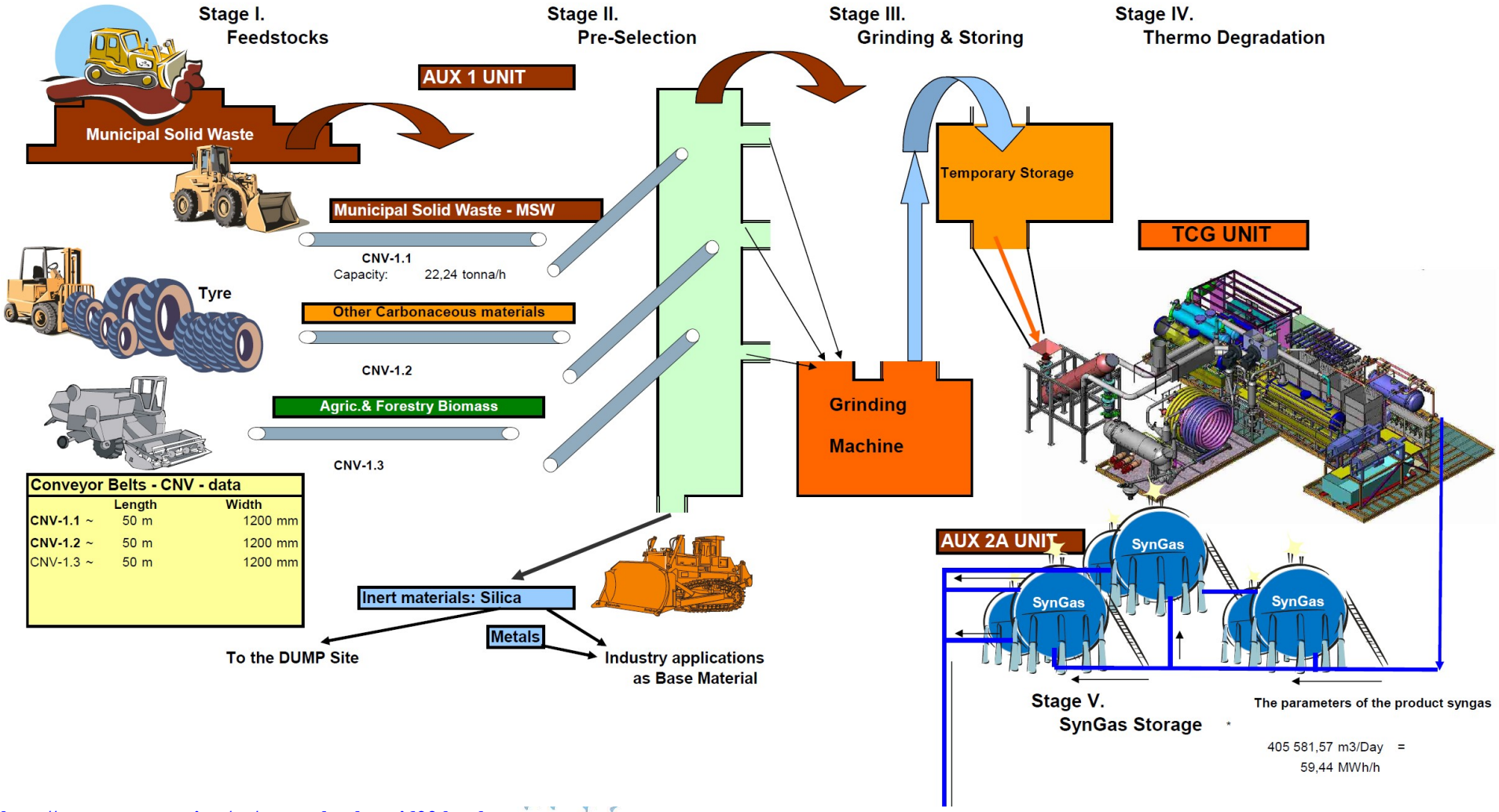

http://www.synergytri.eu/en/tcg_technology-id22.html

Process diagram of TCG-UC EL 500 Plant

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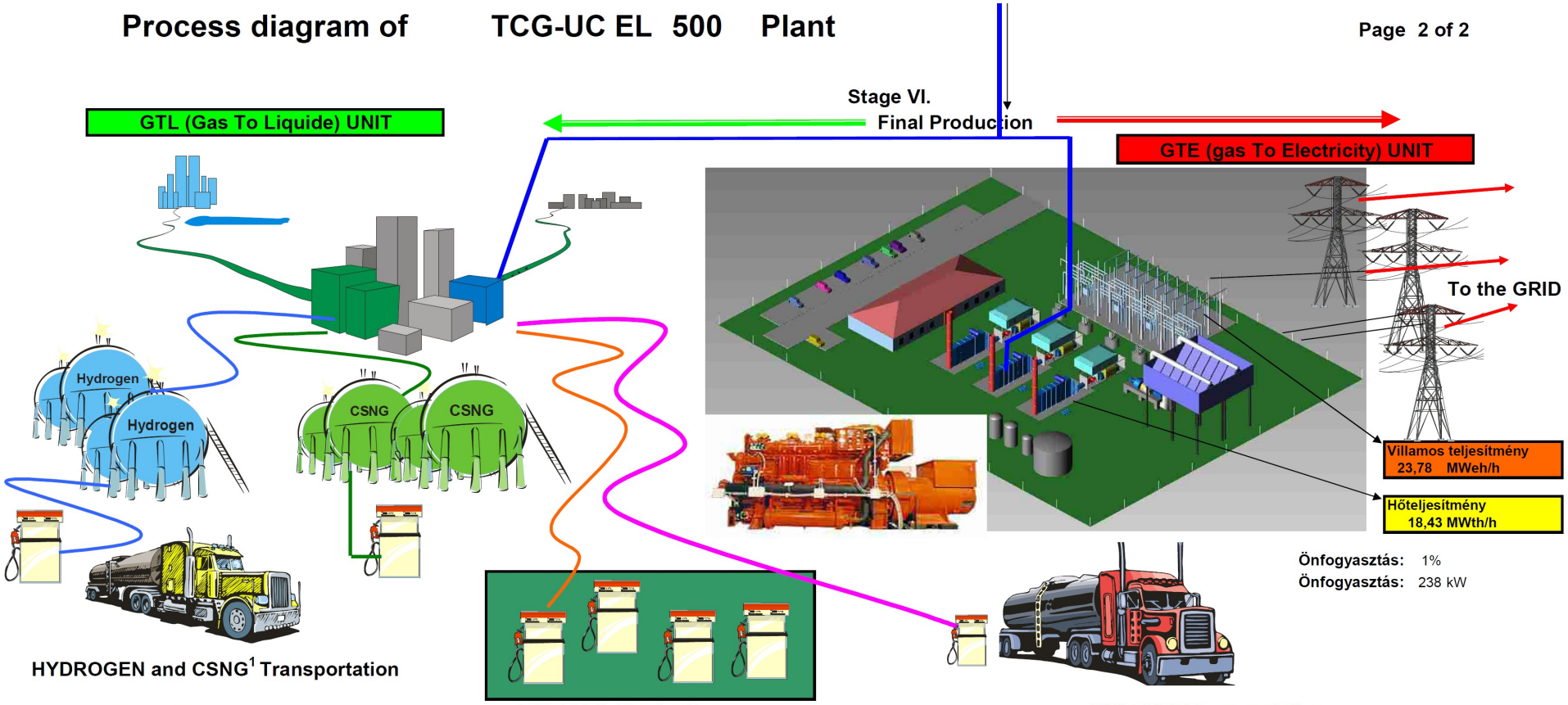


HYDROGEN and CSNG[1] Transportation

The parameters of the product syngas

405 581,57 m3/Day ⟶ 59,44 MWh/h

The Total Quantity of Hydrogen produced

214 958,23 m3/Day

BIO-FUEL Production

Bio-Diesel, Ethanol, Methanol, JET A1, other BIO-FUELS

113 549 Liter/d	**Ethanol/Etanol**
38 155 Liter/d	**Methanol/Metanol**
	or
90 275 liter/day	**Diesel**
	or
95 810 liter/day	**JET A Fuel**

BIO-FUELTransportation

Bio-Diesel, Ethanol, Methanol, JET A1, other BIO-FUELS

1 **CSNG - Compressed Synthetic Natural Gas**

http://www.synergytri.eu/en/tcg_technology-id22.html

Municipal Solid Waste			
500	sTPD DRY		
6 959	BTU/lb =	16 175	kJ/kg
6 959	MM BTU/d=	7 337 042	MJ/d
588	sTPD moist.	13 749	kJ/kg
534	TPD moist.		

Process Diagram of Gasification

TCG ALENA Alternative Energy Applications GmbH.
GLOBAL PROJECT INVEST
Project Name: SAMPLE
Date: 2016.06.15

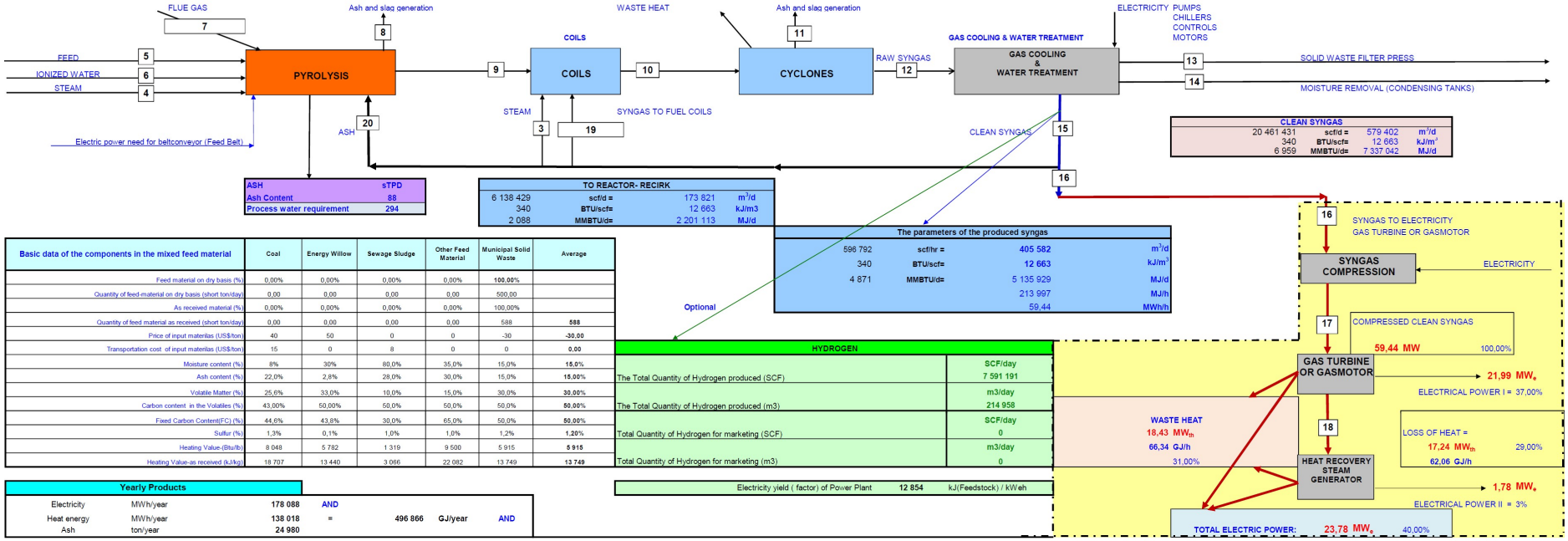
Municipal Solid Waste

with the Licence of GPI LTD

* The modeling is based on the Basic Data provided by the Prospective Purchaser

!! NOT FINAL MODEL !!

Type of TCG Unit: TCG-UC EL 500



CLEAN SYNGAS			
20 461 431	scf/d =	579 402	m³/d
340	BTU/scf=	12 663	kJ/m³
6 959	MMBTU/d=	7 337 042	MJ/d

ASH	sTPD
Ash Content	88
Process water requirement	294

TO REACTOR- RECIRK			
6 138 429	scf/d =	173 821	m³/d
340	BTU/scf=	12 663	kJ/m3
2 088	MMBTU/d=	2 201 113	MJ/d

The parameters of the produced syngas			
596 792	scf/hr =	405 582	m³/d
340	BTU/scf=	12 663	kJ/m³
4 871	MMBTU/d=	5 135 929	MJ/d
		213 997	MJ/h
		59,44	MWh/h

Optional

Basic data of the components in the mixed feed material	Coal	Energy Willow	Sewage Sludge	Other Feed Material	Municipal Solid Waste	Average
Feed material on dry basis (%)	0,00%	0,00%	0,00%	0,00%	100,00%	
Quantity of feed-material on dry basis (short ton/day)	0,00	0,00	0,00	0,00	500,00	
As received material (%)	0,00%	0,00%	0,00%	0,00%	100,00%	
Quantity of feed material as received (short ton/day)	0,00	0,00	0,00	0,00	588	588
Price of input materilas (US$/ton)	40	50	0	0	-30	-30,00
Transportation cost of input materilas (US$/ton)	15	0	8	0	0	0,00
Moisture content (%)	8%	30%	80,0%	35,0%	15,0%	15,0%
Ash content (%)	22,0%	2,8%	28,0%	30,0%	15,0%	15,00%
Volatile Matter (%)	25,6%	33,0%	10,0%	15,0%	30,0%	30,00%
Carbon content in the Volatiles (%)	43,00%	50,00%	50,0%	50,0%	50,0%	50,00%
Fixed Carbon Content(FC) (%)	44,6%	43,8%	30,0%	65,0%	50,0%	50,00%
Sulfur (%)	1,3%	0,1%	1,0%	1,0%	1,2%	1,20%
Heating Value-(Btu/lb)	8 048	5 782	1 319	9 500	5 915	5 915
Heating Value-as received (kJ/kg)	18 707	13 440	3 066	22 082	13 749	13 749

HYDROGEN		
The Total Quantity of Hydrogen produced (SCF)	SCF/day	7 591 191
The Total Quantity of Hydrogen produced (m3)	m3/day	214 958
Total Quantity of Hydrogen for marketing (SCF)	SCF/day	0
Total Quantity of Hydrogen for marketing (m3)	m3/day	0

Yearly Products					
Electricity	MWh/year	178 088	AND		
Heat energy	MWh/year	138 018	=	496 866	GJ/year AND
Ash	ton/year	24 980			

Electricity yield (factor) of Power Plant 12 854 kJ(Feedstock) / kWeh

Results of Technical Modeling

Feedstock		
	500	sTPD DRY
	588	sTPD moist.

Medium Products		
CLEAN SYNGAS	579 402	m3/d
ASH	88,24	sTPD
Process water requirement	294	sTPD

Final Products		
TOTAL ELECTRIC POWER:	23,78	MWe
WASTE HEAT	66,34	GJ/h
HYDROGEN (Optional)	214 958	m3/day

Carbon Conversion Rate:	99,96%
Energy Conversion Rate:	70%

Daily Products		
Ash	80,05	ton/day
Electricity	570,66	MWh/day
Heat energy	1 592,14	GJ/day
HYDROGEN (Optional)	214 958	m3/day

Yearly Products		
Ash	24 980	ton/year
Electricity	178 088	MWh/year
Heat energy	496 866	GJ/year
HYDROGEN (Optional)	67 083 090	m3/year

Results of Financial Modeling

!! NOT FINAL MODEL !!

Capital Expenditures				
Total Project (Entire Project)	154 596 810	USD	=	137 800 414 EUR
Annual Operating Costs				
Total Operation Costs	$8 145 137		=	7 260 196 EUR
Syngas Production for Sale				
30 453 107	revenue US $ per year from all the products		=	27 144 485 EUR
Salary and Labor costs of TCG and Electricity Unit				
Project Labor cost	7 942	US $ per day	=	7 079 EUR/day
Annual EBITDA	24 405 138	US $ EBITDA	=	21 753 606 EUR

Daily Cost	
Total Daily Cost	$51 902 For 30 years of life
Daily Income	
Daily Income of Production	$97 583
Total Daily Income	$113 592
Daily Saldo	**$61 690**

Specific income of Technology:	195	US $/short ton
Specific income of the TCG-UC Project:	227	US $/short ton

*PIP = Plant Installation Period

!! NOT FINAL MODEL !!

RESULT OF PRELIMINARY MODELING

Daily Costs and Incomes

Daily Cost of Feedstock	-$16 009
Daily Total Capital Expenditures	$16 513
Daily Operating Cost	$35 389
Total Daily Cost	**$51 902**
Daily Income of Production	$97 583
Daily Income from Feedstock	$16 009
Total Daily Income	**$113 592**

Project Rate of Return	15%	
Time Frame of Return (Month)*	76,02	* + PIP
Time Frame of Return (Year)*	6,33	* + PIP

Preliminary ProForma — **588 Short ton per Day** — **SAMPLE** — **Gasification Project**

!! NOT FINAL MODEL !!

using the TCG gasification plant and the TCG-UC System

UNICORP USA International Consulting and Servicing Corp.
TCG ALENA Alternative Energy Applications GmbH.
GLOBAL PROJECT INVEST

Feeding material: Municipal Solid Waste
Final Product: ELECTRICITY+HEAT

Type of TCG Unit 500

Date: 2016.06.15

Feedstock Material Municipal Solid Waste
Final Product: ELECTRICITY+HEAT

* The modeling is based on the Basic Data provided by the Prospective Purchaser

!! NOT FINAL MODEL !!

INPUT MATERIALS

500	Dry s.ton/Day	5 915	Btu/Lb =	13 749	kJ/kg
365	Scheduled Days/Year	(27,22)	US $/short ton =	(27)	EUR/ton
85,5%	Overall Availability	-	US $/short ton transportation/handling cost	-	EUR/ton
7 490	Operating hours/year	(27,22)	netto cost of feed stock material US $/short ton	(27)	EUR/ton
156 038	Dry Short Ton/Year	11,83	MM Btu per short ton INPUT MATERIAL=	13,75	GJ/ton
183 574	As Received short ton/Year	(2,30)	Cost ,US $/mmBtu of input material	(1,9)	EUR/GJ
(4 996 086)	Yearly revenue from Solid Waste US $/year			(4 453 279)	EUR
166 536	Feestock quantity tonna/year as received				

Capital Expenditures

Item		Cost (USD)
Total Costs and Fees of Financing		10 113 810
Financial Support (Subsidy)		0
Own resources		0
500	dry tons per day Gasifier	70 000 000
	Ancillary Equipments for Feedstock*	15 046 000
	Ancillary Equipment of the technology altogether	11 136 000
	The price of ELECTRICITY UNIT	40 639 000
Contingencies @	5,60%	7 662 000
	Total Project (Entire Project)	154 596 810

Payment schedule

Installment(%)	Sum (USD)	Sum (EUR)	Proposed period of payment	
40%	61 838 724	55 120 165	In 3 weeks after contracting	
30%	46 379 043	41 340 124	120	days
20%	30 919 362	27 560 083	180	days
10%	15 459 681	13 780 041	180	days
Total	154 596 810	137 800 414		

154 596 810 USD = 137 800 414 EUR
137 800 414 EUR

Daily cost $18 512,8 USD = 14 719 EUR
14 718,7 EUR

Syngas Production for Sale

1 520 174	Syngas MM btu per year =	1 602 795	GJ	Energy Content of the produced SynGas Yearly
9,13	net MM btu/ton of as received input material	9,6243	GJ/ton	The Heat content of the feed stock/ton
126 571 868	produced syngas cubic meter per year			
30 453 107	revenue US $ per year from all the products =		27 144 485	EUR
24 041 927	revenue US $s per year from SynGas =		21 429 857	EUR
19 233 542	revenue US $ per year from SNG =		17 143 885	EUR
24 932 369	revenue US $ per year from Electricity =		22 223 555	EUR
33 664 021	revenue US $ per year from ETHANOL =		30 006 544	EUR
3 771 283	revenue US $ per year from METHANOL =		3 361 546	EUR
25 115 818	revenue US $ per year from JET A-1 =		22 387 073	EUR
27 834 482	revenue US $ per year from DIESEL =		24 810 364	EUR
-	revenue US $ per year from Hydrogen =		-	EUR
5 520 739	revenue US $ per year from STEAM =		4 920 930	EUR

Annual Operating Costs

	O&M cost of the Gasifiers	$ 532 061	0,35	US $/MM Btu	474 254	EUR
	O&M cost of the Electric unit	$ 456 052	0,300	US $/MM Btu	406 504	EUR
	Production cost of Hydrogen	$ -	0,002	US$/scf	0,06	EUR/m3
	Cost of Ash Disposal	$ 499 609	20,00	US $/t	445 328	EUR
Electricity @ 1,44	Megawatt	$ 1 509 944	0,14	US $/KWH	1 345 894	EUR
	Spare Parts (@ 1% of Cap. Exp.)	$ 1 278 333			1 139 447	EUR
	G&A (@ 1% of Cap. Exp.)	$ 1 278 333			1 139 447	EUR
	Insurance (@0,5% of Cap. Exp.)	$ 639 166			569 723	EUR
	Contingency on above at: 10,00%	619 350			552 060	EUR
	Cost of preselection	1 332 290			1 187 541	EUR
	Total Operation Costs	$ 8 145 137			7 260 196	EUR

Daily cost $26 100

Daily cost of "Operation Cost Total" in continuous operation $4 329 955 — Daily cost $13 875
Part of "Operation Cost Total" in case of emergency $3 815 182 — Daily cost $12 225

Annual EBITDA

30 453 107	US $ Gross Revenue	27 144 485 EUR
(4 996 086)	US $ Feed stock Cost	(4 453 279) EUR
-	US $ Income from Drying Fee	0 EUR
35 449 194	US $ Net Revenue	31 597 764 EUR
2 898 919	US $ Labor Cost	2 583 961 EUR
8 145 137	US $ Operation Cost	7 260 196 EUR
24 405 138		21 753 606 EUR

Note:
609 062 148 = 20 Year Gross Revenues from Syngas
488 102 765 = 20 Year Net Revenues from project

Capital

154 596 810	US $ Investment
0,02780392	US $/kWh cost of unit of electricity
2,2067	US $/GJ cost of heat

Rates of Exchange	HUF	USD	EUR	EUR
HUF	1	0,003575515	0,003187048	0,003187048
USD	279,68	1	0,891353539	0,891353539
EUR	313,77	1,121889302	1	1
EUR	313,77	1,121889302	1	1

Salary and Labor costs of TCG and Electricity Unit

	Labor cost					
1 858	Labor cost of TCG US	US $ per day	1 Engineer(s) +	18	Worker(s)	
6	Operators per day at GTE (incl supv)		1 Engineer(s) +	5	Worker(s)	
12,68	Average US $ per hour (loaded)		11,30 EUR/h	271	EUR/day	
8	daily working hours					
0,34	Ratio of bonuses compared to the 100%					
619,08	Total allowances/benefits per day	US $ per day		552	EUR/day	
2 467	Labor cost	US $ per day		2 199	EUR/day	
5 475	Labor cost of preselection unit	US $ per day		4 880	EUR/day	
7 942	Project Labor cost	US $ per day		7 079	EUR/day	

Daily Cost

Daily Cost of Feedstock	-$16 009
Daily Total Capital Expenditures	$16 513 For 30 years of life
Daily Operating Cost	$35 389
Total Daily Cost	$51 902 For 30 years of life

Daily Income

Daily Income of Production	$97 583
Daily Income from Feedstock	$16 009
Total Daily Income	$113 592
Daily Saldo	$61 690

Yearly

Pro Forma ($000)

	Year (-1:0) Constr.+Operat.	Year 1	Year 2	Year 3	Year 4	Year 5	Year 6	Year 7	Year 8	Year 9	Year 10	Year 11	Year 12	Year 13	Year 14	Year 15	Year 16	Year 17	Year 18	Year 19	Year 20	Total
Earnings before interest, tax, depreciation & amortization		24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	488 103
Capital Investment	154 597																					
Pre-TaxCash Flow	(154 597)	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	24 405	488 103
Cum Pre-Tax Cash Flow	(154 597)	(130 192)	(105 787)	(81 381)	(56 976)	(32 571)	(8 166)	16 239	40 644	65 049	89 455	113 860	138 265	162 670	187 075	211 480	235 885	260 291	284 696	309 101	333 506	
Time Length of return of investment	6,33	year																				
Project Rate of Return	15%	Before tax																				

!! NOT FINAL MODEL !!

SYNERGY GROUP

Brief Summary of TCG-UC EL500 SAMPLE Project

Project Name (Place & Final Product):	SAMPLE
Name of Input (feed) Material	Municipal Solid Waste
Contractor/Supplier:	TCG ALENA Alternative Energy Applications GmbH.
Date:	2016.06.15

1. Brief Description of the Technology

The objective of this project is to design and establish a TCG-UC Waste To Green Energy Power Plant capable of producing electricity from the specific feedstock material as determined by the purchaser according to the site specific data and information, and the availability of feedstock material. The plant will produce an extremely clean synthetic gas (mostly H2 and CO) intended to be utilized in a gas motor or turbine and generator set to produce electricity that either independently or in connected to the national grid would service the required energy needs of a larger community. The TCG-UC W2GE project will serve the energy needs of a town, industrial firms, or recreational complex incorporating sports, wellness, hotel and other facilities. The undisputable advantages of the TCG technology against other existing, superficially-similar systems is that the TCG is uniquely designed and is capable of utilizing a very broad range of materials (containing acceptable carbonaceous content) either as a single feed stock or in any combination. This list of potential feed stocks includes: biomass from agriculture, solid waste from communities, used tyres and many other carbonaceous materials

2. Basic Parameters of the Project

Quantity of total input material (dry basis)	500	Dry s.ton/Day	=	588		sTPD moist.
	156 038	Dry Short Ton/Year	=	183 574		As Received short ton/Year
Scheduled Days/Year	365		=	8 760	Hours	
Overall Availability	85,50%	that means		7 490	Operating hours/year	
Energy Content	16 175	kJ/kg	=	7 337 042	MJ/d	
Selling price of Electricity	0,14	$/kWh =	0,1248	EUR/kWh		
Cost of Electricity	0,14	$/kWh =	0,1248	EUR/kWh		
Acceptance fee of MSW (Income)	-30,00	US$/ton				
Transportation fee	0,00	USD/tonna				
Selling price of Heat	0,04	$/kWh =	11,111	US$/GJ		
Engineers' salary	12,00	US$/hour				
Workers' salary	9,00	US$/hour				

3. Capital Expenditures

Total Project (Entire Project)	$154 596 810	=	137 800 414 € =

4. Final Products

Electric Power	23,78	MWe	=	178 088	MWh/year
Heat energy	18,43	MWth	=	138 018	MWh/year = 496 866 GJ/year

5. Yearly Income

MSW	166 536	TPD moist.	X	30,00	US$/ton	=	$4 996 086
Electricity	178 088	MWh/year	X	0,14	$/kWh =		$24 932 369
Heat energy	138 018	MWh/year	X	0,04	$/kWh =		$5 520 739
Total							**$35 449 194**

6. Annual Operating Costs

Total Operation Costs	$8 145 137
Salary and Labor costs of TCG and Electricity Unit	$2 898 919

7. Annual EBITDA

US $ EBITDA	**$24 405 138**

8. Financial results

Project Rate of Return	15%	
Time Length of return of investment	6,33 year	* + PIP

*PIP = Plant Installation Period

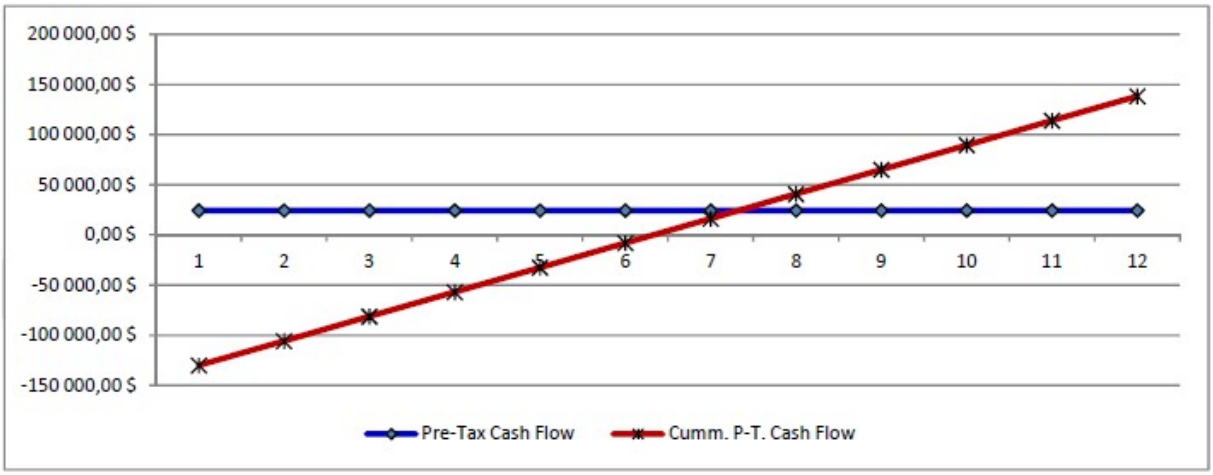
CASH-FLOW OF TCG-UC EL500 SAMPLE **!! NOT FINAL MODEL !!**

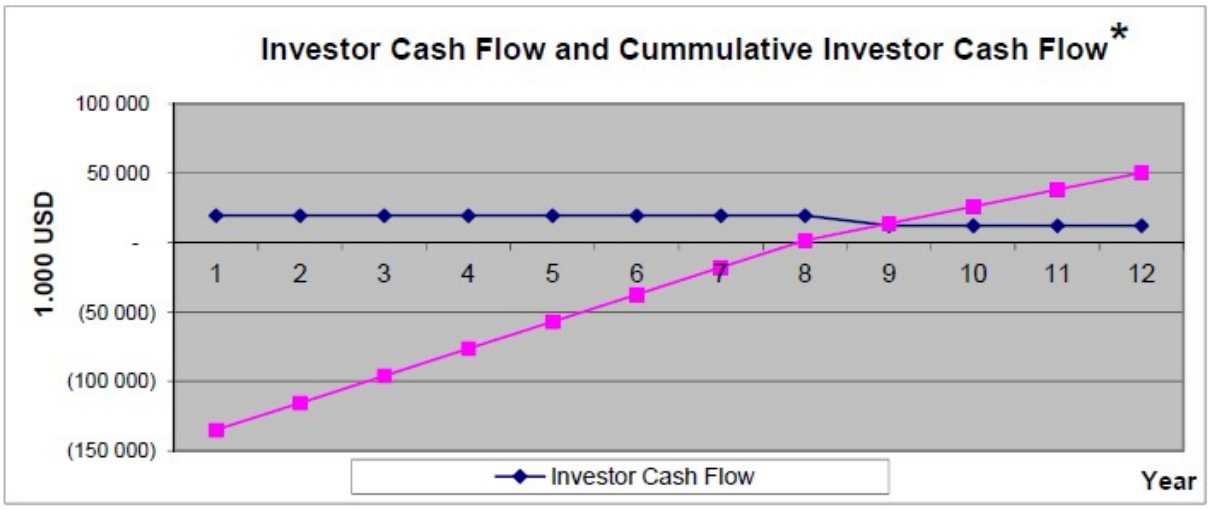
Pro Forma ($000)

	Year (-1;0) Constr.+Operat.	Year 1	Year 2	Year 3	Year 4	Year 5	Year 6
Earnings before interest, tax, depreciation & amortization		24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14
Capital Investment	154 596,81						
Pre-TaxCash Flow	-154 596,81	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14
Cum Pre-Tax Cash Flow	-154 596,81	-130 191,67	-105 786,53	-81 381,40	-56 976,26	-32 571,12	-8 165,98

Time Length of return of investment	6,33	year
Project Rate of Return	14,78%	Before tax

Year 7	Year 8	Year 9	Year 10	Year 11	Year 12	Year 13	Year 14	Year 15	Year 16	Year 17
24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,1
24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,14	24 405,1
16 239,16	40 644,30	65 049,43	89 454,57	113 859,71	138 264,85	162 669,99	187 075,13	211 480,26	235 885,40	260 290,5





The salability of the produced electricity – manufactured by TCG-UC W2E Power Plants - is guaranteed in Europe.
The Green Energy production is highly supported by the Green Energy Sections of the Law of Energy that set priority and the obligatory purchasing of the Green Electricity Energy.

Visit the video in our site: **http://www.synergytri.eu/en/tcg_technology-id39.html**

In case of any inqueries.

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